

A PHYSICAL ANALYSIS OF THE COUPLED AEROSOL-LIGHT BEAM SYSTEM

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ABSTRACT

The coupled aerosol-light beam system is studied. For water droplets the energy balance equation is solved by numerical integrations. A comparison between the present results and previous results is offered for the maximum temperature rise of the water droplets. The effect of the beam intensity on the droplet heating is studied. The mass flux and the vaporization rate are investigated in both the low and high energy case. A new parameter describing the droplet temperature decay is defined.

INTRODUCTION

The problem of the heating and vaporization of absorbing droplets in intense light beams has been studied by a number of investigators [1-3]. In a previous investigation [1], an approximate solution was obtained for the energy balance in a spherical fluid droplet irradiated by a pulsed light beam. The vapor kinetic energy term has been omitted from the energy conservation equation. Furthermore, the mass flux has been expanded in a power series up to the second order. The results for this second-order approximation is compared with the corresponding present results obtained in our paper using numerical integration solution.

In many applications of practical importance, and at high irradiance, the aerosol heating, vaporization, and conductive heat losses are the dominant energy dissipation mechanisms for the propagating beam. As the pulse energy increases, the vaporization is the dominant energy draining mechanism. When the droplet radius doesn't exceed $10\ \mu\text{m}$ and the incident flux level is in the range of $10^3 - 10^5\ \text{W}/\text{cm}^2$, diffusive evaporation is the dominant process in the high-energy laser interaction with water aerosols. By way of contrast, for fluxes reaching $10^7\ \text{W}/\text{cm}^2$, explosive vaporization and shock formation become important. The effects of nonuniform droplet heating and the localization of the beam at the droplet walls are significant at short times and for larger droplets whose radius exceed $10\ \mu\text{m}$.

In the present work, we consider the heating and vaporization of absorbing water droplets in an intense pulsed light. The droplets absorb energy from the propagated light so that their temperature rises as a

function of the droplet size beam intensity and the pulse length. Due to the rise of the droplets temperature, they vaporize and heat the ambient medium conductively. In other words, the amount of the energy absorbed by the droplet, during passage of the pulse, is deposited into heating the droplet, vaporizing the droplet, and heating the surrounding medium.

In this paper, we study the effects of the beam parameters, as well as the droplet size, on the temperature rise of the water droplets. The energy balance equation, using the exact expression of the mass flux, is solved using the numerical integrations. The results of the present numerical solution show that the previous second-order approximation breaks down except for the cases discussed later.

For a more rigorous solution of the energy conservation equation, the vapor kinetic energy term and the droplet shrinkage term are included. The former term has an appropriate contribution to the droplet temperature in the high energy case. For the sake of completeness, we include the second discussed previously by Davies and Brock [4]. This energy term is about 30% of the droplet heating energy in the low energy case[5]; it becomes comparable with the heating energy case, but then the energies of shrinkage, heating, and conduction are small compared with the vaporization energy.

In this paper, we study the effect of the beam intensity on the droplet heating through a parameter defined as the critical beam intensity which is required to heat the water droplet up to its boiling temperature. The mass flux and the vaporization rate are studied carefully through the effects of the beam parameters and droplet size. The

temperature decay time, as a new parameter, is defined in this paper. It is investigated accurately as a function of the beam parameters and droplet radius.

Droplet temperature rise

The time-dependent droplet temperature T , may be obtained from the solution to an energy-conservation equation that describes the balance between absorption and dissipative processes within a droplet of radius r . The energy-balance is [1]

$$\frac{4}{3} \pi \sigma^3 \rho C \frac{\partial T}{\partial t} + 4 \pi \sigma^2 [mL + mC(T-T_0)] - K \left(\frac{\partial T}{\partial r} \right)_{r=\sigma} + \frac{m^3}{2\rho^2} = \frac{4}{3} \pi \sigma^3 \alpha I, \quad (1)$$

where ρ , C , L , and α are, respectively, the droplet density specific heat, heat of evaporation, and the frequency-dependent bulk absorption coefficient; ρ' , T_0 , and K are, resultively, the density, temperature, and the thermal conductivity of the surrounding medium. I is the intensity of the beam and m is the mass flux.

The term $4 \pi \sigma^2 mC(T-T_0)$ is the droplet shrinkage energy term which is included in this paper for the sake of completeness. The term $4\pi\sigma^2[mL + mC(T-T_0)]$ represents an effective heat of evaporation.

In the quasi-steady approximation, we use[1]

$$m = \frac{D}{\sigma} \left[\frac{1 - Y_0}{1 - Y_0 \exp \left(\frac{LM}{RT_0} - \frac{LM}{RT} \right)} \right] \quad (2)$$

$$K \left(\frac{\partial T}{\partial r} \right)_{r=\sigma} = \frac{mC_p(T-T_0)}{\exp(mC_p\sigma/K)-1} \quad (3)$$

where D , M , and C_p are the vapor diffusion coefficient, molecular weight, and specific heat, respectively. R is ideal gas constant, and Y_0 is the ambient vapor mass fraction.

Inserting Eq.(3) into Eq.(1), and using the dimensionless variable $X(t) = [T(t)-T_0]/T_0$, we obtained the following energy balance equation for water droplets

$$\frac{dX(t)}{dt} = 8 \times 10^{-10} \alpha I - 1.2 \times 10^{-9} \frac{m^3(t)}{\sigma \rho^2} - \frac{m(t)}{\sigma} - 3 \times 10^{-3} \frac{\sigma \rho^2}{m(t)X(t)} - \frac{7.2 \times 10^{-7} m(t)C_p X(t)}{\sigma [\exp\{m(t)C_p/\sigma K\}-1]} \quad (4)$$

where $T_0 = 300$ °K, $m(t)$ is computed for water droplet from Eq.(2) as

$$m(t) = \frac{3 \times 10^{-5}}{\sigma} \ln \left[\frac{0.9862}{1 - 0.0138 \exp(B)} \right], \quad (5-a)$$

and

$$B = 16.32 \frac{X(t)}{1 + X(t)} \quad (5-b)$$

Equation (4) is solved numerically using an intensity profile $I(t)$ of the form

$$I(t) = I_0, \quad 0 \leq t \leq t_p, \\ = 0, \quad \text{elsewhere} \quad (6)$$

The time step Δt is selected not more than 10^{-7} sec, for pulse lengths not less than $5 \mu\text{sec}$, to give a high accuracy for the time-dependent droplet temperature. This achieves stability in the numerical integration scheme. The pulse length t_p is chosen so that $t_p \gg t_h$, where t_h is the droplet heating time: the time scale for the droplet to approach a steady state temperature [1].

For water droplet we estimated, at $t_0 = 300$ oK, the droplet heating time which is obtained as a function of droplet radius in following formula

$$\tau_h(\sigma, I) = 3.4 \times 10^7 \sigma^2 [3.2 + \sigma^2 \alpha I]^{-1/2}, \text{ sec} \quad (7)$$

where σ^2 is in m^2 , and $(\sigma^2 \alpha I)$ is in W/m .

Figure (1) illustrates the droplet temperature rise $\Delta T(t)$ versus normalized time t/t_p for the selected value of droplet radius and beam intensity αI for a $5 \mu\text{sec}$ pulses. a first feature of interest is that, the temperature of the larger droplet radii increases more faster with time than the temperature of the smallest ones. This occurs during the passage of the pulse up to a maximum temperature rise ΔT_m at the pulse end ($t=t_p$). It is clear that the droplets of small sizes reach a steady state temperature during the heating phase. This is because, according to Eq. (7), such droplets have heating time $t_h \ll t_p$.

Table 1. shows a comparison between our present results, obtained through numerical-integration solution, and the results of Ref. [1] obtained by the second-order solution. We can find that the previous results are in good agreement with the present results for $16 > \sigma^2 \alpha I$ (W/m) ≥ 1 . It is clear that the second-order approximation used in Ref.[1] is excellent approximation for $\sigma^2 \alpha I = \text{W/m}$.

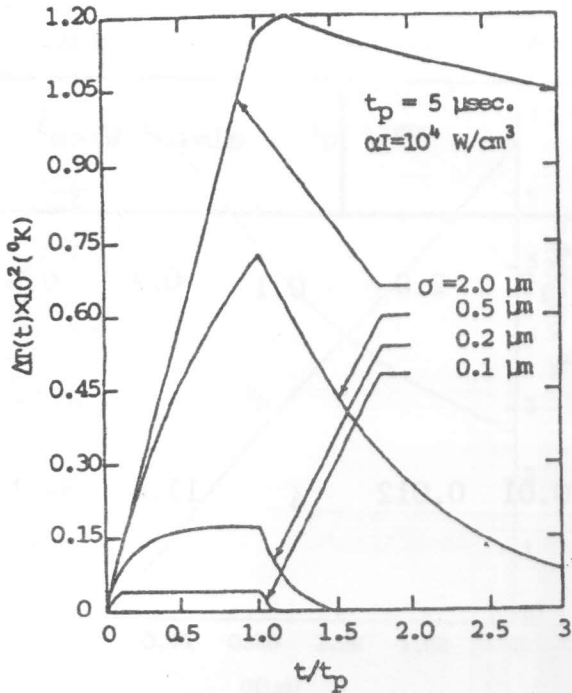


Figure 1. Variations of the droplet temperature rise with normalized time.

Otherwise, the numerical solution numerical values for ΔT_m less than those of Ref.[1] which obtained by the second-order solution.

Critical beam intensity

Figure (2) gives the intensity dependence of the maximum temperature rise ΔT_m , for selected values of the droplet radii. It is evident that for a given droplet size there is a critical beam intensity $\alpha I_c(\sigma)$ required to heat droplet up to boiling temperature T_B . The correlation between αI_c (σ) and σ is given in Figure (3). The feature of interest is that all droplets having radii more than $2 \mu m$ need approximately the same critical beam intensity to heat up to T_B . For droplets with $0.3 \leq \sigma(\mu m) \leq 1$, the critical beam intensity is inversely proportional to σ with a negative rate $(\partial^2 \alpha I_c) / \partial \sigma^2$. All droplet less than $0.3 \mu m$ have a linear proportionality with the critical intensity.

Steady-state vaporization rate

For water droplets, we estimate the droplet decay time τ_d [1], as a function of the intensity, αI under the final following from

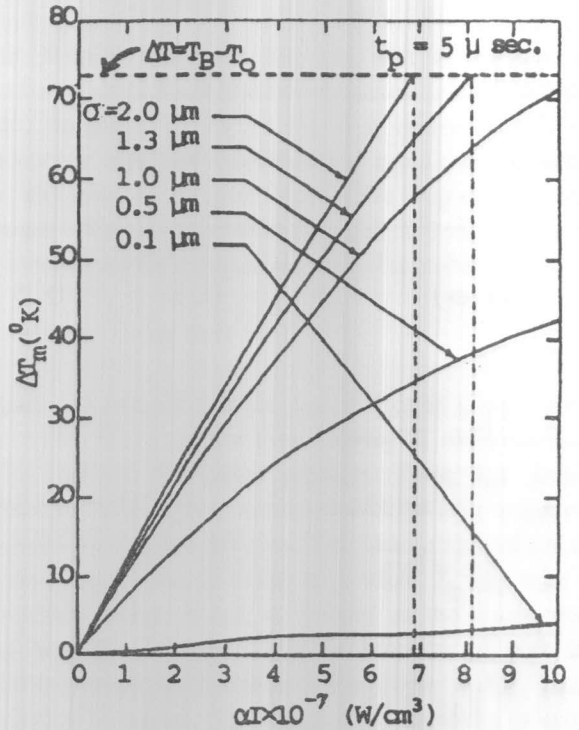


Figure 2. Variations of the maximum droplet temperature rise with beam intensity.

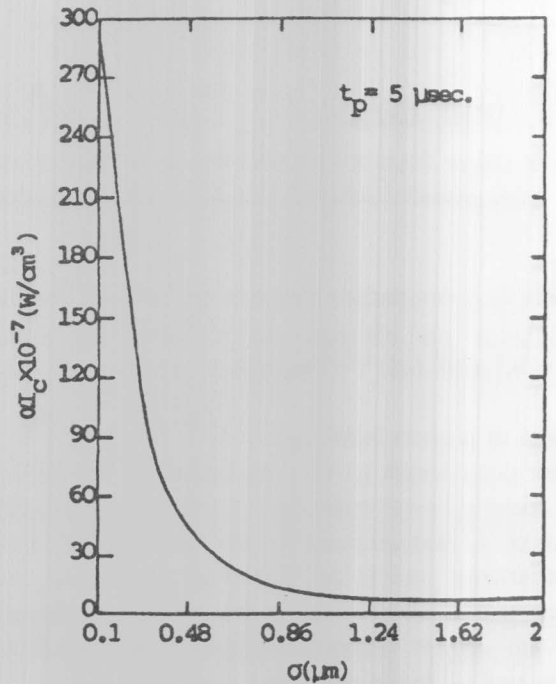


Figure 3. Variations of the critical beam.

	$\alpha I = 10^4 \text{ W/cm}^3$				$\alpha I = 10^8 \text{ W/cm}^3$		
$\sigma (\mu\text{m})$	0.1	0.5	1.0	2.0	0.1	0.2	0.4
The present results	4×10^{-4}	7.3×10^{-3}	0.01	0.012	4	13.4	34.1
$\Delta T_m (^\circ\text{K})$							
Ref. [1] results	3×10^{-3}	0.07	0.10	0.118	4	14	41
$\Delta T_m (^\circ\text{K})$							
$\sigma^2 \alpha I (\text{W/m})$	10^{-4}	2.5×10^{-3}	0.01	0.040	1	4	16

Table 1. A comparison between our present results and the results of Ref. [1].

$$\tau_d = 9.5 \times 10^3 (\alpha I)^{-1}, \text{ sec} \quad (8)$$

$$V_R(\sigma, I) = 4\pi\sigma^2 m(\sigma, I). \quad (15)$$

where αI is given in W/cm^3 .

For pulse length $t_p \ll \tau_d$, the radius of the droplet may be taken to be approximately constant, i.e. $\sigma(t) = \sigma(0)$. The droplet is characterized by the ambient pressure and temperature prior to the arrival of the pulse at $t=0$. For times $t > 0$ the droplet energy from the beam, hence, both of the droplet temperature and vaporization rate is increased up to the pulse end where $t = t_p$.

The vaporization rate V_R , as a function of droplet radius σ , is given by

When the droplet radius and the beam intensity are selected so that, according to Eq.(9), $\tau_h \ll t_p$, the droplet temperature reaches to its steady state. This case leads to steady state values for both $m(\sigma, I)$ and $V_R(\sigma, I)$. Figures 4 and 5 show the variations of both the steady state vaporization rate and mass flux with the droplet radius for the low and high energy cases.

In Figure (4) it is clear that, in the low energy case, the

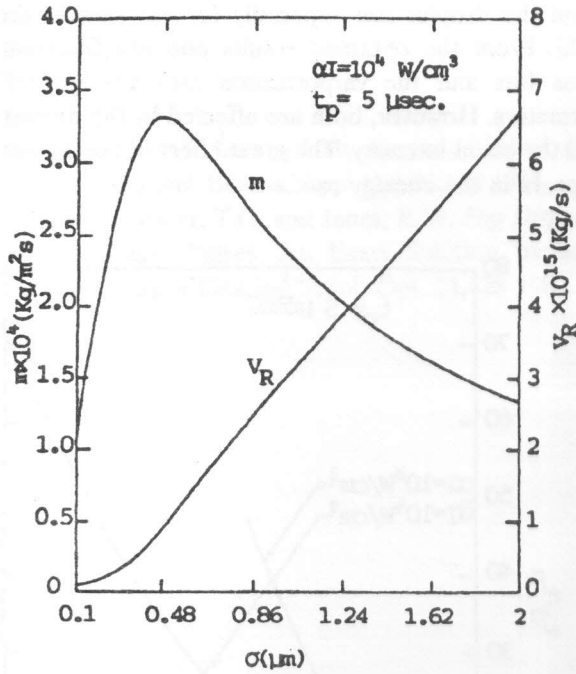


Figure 4. Variations of the mass flux m and vaporization rate V_R with droplet radius, $\alpha I = 10^4 \text{ W/cm}^3$.

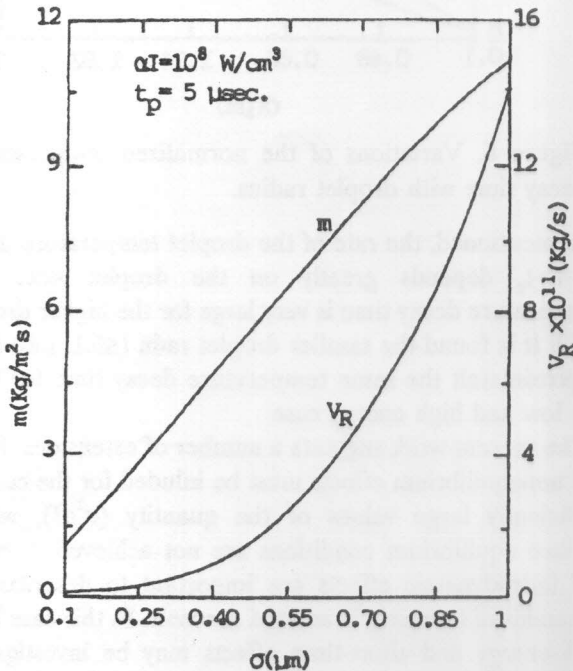


Figure 5. Same as in figure 4, but with $\alpha I = 10^8 \text{ W/cm}^3$.

mass flux has a positive rapid correlation with the smallest droplet radii, and a negative slow correlation with the

larger droplet radii. for droplets with $\sigma > 0.3 \mu\text{m}$, the vaporization rate has a linear dependence with the droplet radius. As shown in Figure (5), it is evident that, in the high energy case, the mass flux has a positive correlation with all selected droplet sizes. The vaporization rate increases with a positive rate $(\partial^2 V_R)/(\partial \sigma^2)$ while the mass flux increases with a negative rate $(\partial^2 m)/(\partial \sigma^2)$.

Temperature decay time

Figure (1) reveals that the water droplet temperature is increased for times greater than zero up to a maximum value at the end of the pulse passage. Then, the droplet temperature begins to decrease with a rate negatively correlated to the droplet size. The time, required for the droplet temperature to decay to a value T_f very close to the ambient temperature, is defined as the temperature decay time t_d . This parameter is function of both the maximum temperature rise and the droplet radius. t_d may be selected to equal AT_o , where A is very close to unity.

Now, for small droplet sizes, $\sigma < 0.1 \mu\text{m}$, one can formulate an expression for the parameter t_d . When σ is so small that one can neglect the conducting, kinetic, and shrinkage energy terms, the energy balance equation, for $t > t_p$, can be written as

$$\frac{4}{3} \pi \sigma^3 \rho C \frac{dT}{dt} + 4\pi \sigma^2 mL = 0, \tag{16}$$

where m may be approximated, for small values of the dimensionless variable X , to be in the following form

$$m = \frac{DLMY_o X}{\sigma RT_o(1-Y_o)} \tag{17}$$

Substitute m from Eq.(17) into Eq.(16), using the dimensionless variable X instead of T , we obtain

$$\rho C T_o \frac{dX}{dt} + \frac{3DL^2MY_o}{\sigma^2 RT_o(1-Y_o)} X = 0. \tag{18}$$

For water droplet Eq.(18) can be integrated and rewritten as

$$X_f \int_{X_m} \frac{dX}{X} = - \frac{4 \times 10^{-8}}{\sigma^2} \int_{t_p}^{t_d} dt,$$

$$t_d = 2.5 \times 10^7 \sigma^2 \ln \frac{X_m}{X_f} + t_p, \tag{19}$$

Where X_f is the dimensionless variable, and the maximum

dimensionless variable ($X_m = \Delta T_m/T_o$) can be obtained by rewriting Eq.(18) for the time range $0 \leq t \leq t_p$. Hence, we have

$$\rho C T_o \frac{dX}{dt} + \frac{3D^2 L M Y_o X}{\sigma^2 R T_o (1-Y_o)} = \alpha I. \quad (20)$$

For water droplets, integration of Eq.(20) yields the following formula

$$X_m \int_0^{X_m} \frac{dX}{8 \times 10^{-10} \alpha I - \frac{3 \times 10^{-7}}{\sigma^2} X} = \int_0^{t_p} dt,$$

which gives the maximum dimensionless variable as

$$x_m = 2.7 \times 10^3 \sigma^2 \alpha I [1 - \exp(-3 \times 10^{-7} t_p / \sigma^2)]. \quad (21)$$

The final dimensionless variable X_f can be easily obtained by using $T_f = AT_o$. This leads to

$$X_f = \frac{T_f - T_o}{T_o} = A - 1 \quad (22)$$

Equations (22),(21), and (19) provide three equations which determine the temperature decay time t_d in terms of the plotted radius, pulse length, and the beam intensity.

In Figure (6) we plotted the variation of the normalized temperature decay time (t_d/t_p) with the droplet radius for the selected values of αI . The plotted results are obtained using the numerical integration of the energy balance equation, Eq.(4), under the condition of $x_f = A-1 = 10^{-8}$. It is clear from Figure (6). that the parameter t_d increases for the larger droplet sizes. The rate ($\partial t_d / \partial \sigma$) is positively correlated with the beam intensity.

CONCLUSION

In this paper, we have studied carefully the interaction between the water droplets and a monochromatic pulsed beam of electromagnetic radiation. The coupled nonlinear differential equations describing the energy and mass conservation are numerically solved.

The results of the present work reveal that the second-order solutions obtained in Ref.[1] are in agreement with the present numerical solution for the condition $16 > \sigma^2 \alpha I (W/m) \leq 1$. The excellent agreement occurred for the condition $\sigma^2 \alpha I = 1 W/m$.

The critical beam intensity, required to heat the droplet

up to the boiling temperature, has a great dependence upon the droplet size especially for the smaller droplet radii. From the obtained results one can find that the mass flux and the vaporization rate are independent parameters. However, both are affected by the droplet size and the beam intensity. The great effect of the droplet size appears in the energy case.

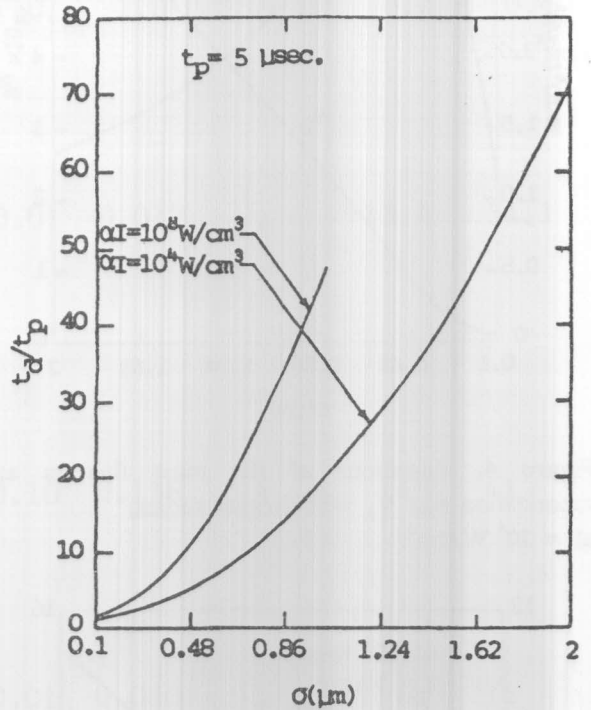


Figure 6. Variations of the normalized temperature decay time with droplet radius.

as mentioned, the rate of the droplet temperature decay at $t > t_p$ depends greatly on the droplet size. The temperature decay time is very large for the higher droplet radii. It is found the smaller droplet radii ($\leq 0.1 \mu m$) have approximately the same temperature decay time for both the low and high energy case.

The present work suggests a number of extensions. First, the nonequilibrium effects must be included for the case of sufficiently large values of the quantity ($\sigma^2 \alpha I$), where surface equilibrium conditions are not achieved. Second, the hydrodynamic effects are important to describe the dynamics of intensely irradiated aerosols. In this case both high-energy and short-time effects may be investigated. Finally, one can consider the more general problem of beam propagation in a poly-disperse size distribution which require knowledge of the particle concentration per unit volume, the particle-size distribution function, and the

single-particle extinction coefficient.

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